

PROCESS SYSTEMS INTERNATIONAL, INC. WESTBOROUGH, MA					ENGINEERING CALCULATIONS	NO: V049-1-096 PAGE 1 OF 15
REV.	DEO #	DATE	BY:	CHECK	TITLE: Regen. System Process Calculations	
0	130	4/19/96	D. Moore	D. McW		
1	416	1/16/97	D. Moore	D. McW		
					BY: D. Moore	DEPT.: 744
<u>PROJECT: LIGO</u>					<u>PROJECT NO: V59049</u>	
<u>PURPOSE:</u> Determine process requirements for the 80K pump regen. heaters, to estimate the warmup time (time to reach 150 C) for the pump under wintertime conditions in Washington, and to determine insulation thickness for personnel protection.						
<u>METHOD:</u> Standard heat transfer manual calcs. and on spreadsheet format.						
JAN 21 1997						
<u>ASSUMPTIONS:</u> Used weather conditions for Kennewick, Washington: 15 deg. F dry bulb (Above this temperature 97.5% of the time.) For personnel protection, used summertime design temperature of 96 deg. F dry bulb (Below this temperature 97.5% of the time), and light (5 mph) breeze.						
<u>INPUTS:</u> Max. regen. flowrate = 100 gm/sec. for long pump; 50 gm/sec. for short pump. N2 temperature from the vaporizer = -5 deg. F (20 deg. F approach temp. specified by mfg.)						
<u>REFERENCES:</u>						
<u>CALCULATIONS:</u> See attached.						
<u>CONCLUSIONS:</u> Long pump heater size: 25 kw adequate. Short pump heater size: 12 kw adequate. Estimated warmup times, including liquid vaporization: long pump = 16.75 hrs., short pump = 8.0 hrs. Max. surface temperature of insul. = 115 deg. F is acceptable for personnel protection.						
<u>NOTES:</u>						

PROCESS SYSTEMS INTERNATIONAL, INC. WESTBOROUGH, MA	ENGINEERING CALCULATIONS	NO: V049-1-096
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PROJECT: LIGO VACUUM EQUIPMENT	PROJECT NO:	V59049
CALCULATION TITLE: Regen. System Process Calculations		

REVISION HISTORY

- Rev. 0 Original Issue -April 19, 1996
- Rev. 1 Revised to determine insulation thickness for pesonnel protection

80K Pump Regeneration Process Calculations

Sizing of Regen Heaters:

Heaters must be sized to deliver hot N_2 gas to the 80K pumps. The 80K pumps are to be heated to $302^\circ F$ ($150^\circ C$). Assuming a $20^\circ F$ approach temperature, the gas temperature entering the cryopump should be about $325^\circ F$.

Wintertime Operation:

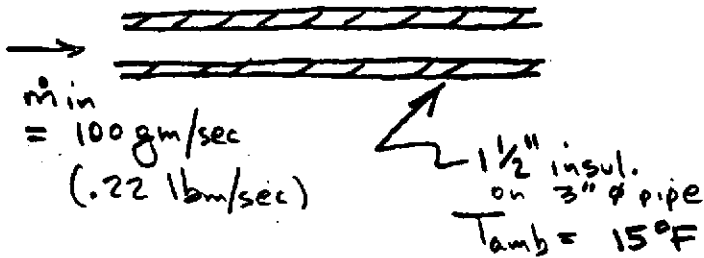
Using available design data, size the heater for $15^\circ F$ dry bulb wintertime conditions (see Attachment 1). Assume a 10 m.p.h. wind blowing across the line supplying the regen. gas to the cryopump. \therefore Calculate the temperature exiting the heater in order to overcome heat losses from the supply line.

50 SHEETS
22-141
100 SHEETS
22-142
200 SHEETS
22-144



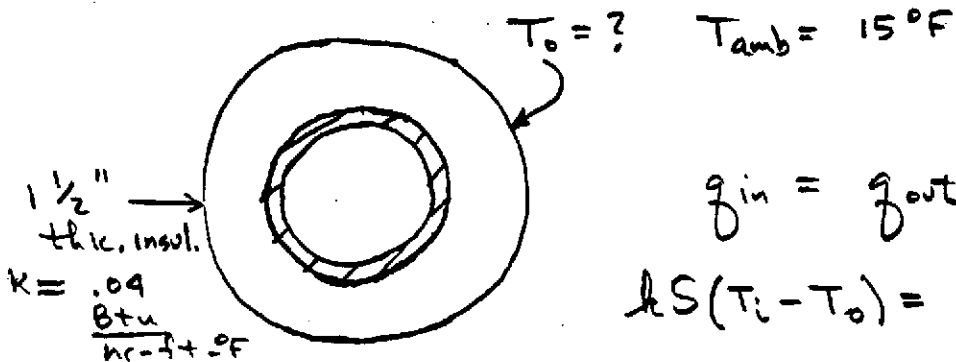
Heat Loss thru 60 ft. of regen pipe:

Long pump:



$$T_{out} = 325^\circ\text{F}$$

$$T_{in} = ?$$



$$\dot{q}_{in} = \dot{q}_{out}$$

$$kS(T_i - T_o) = hA(T_o - T_{amb})$$

$$S = \frac{2\pi L}{\ln(r_o/r_i)}$$

$$= \frac{2\pi(1.0)}{\ln(6.5/3.5)} = 10.15 \text{ ft}$$

Assume 10 mph wind

$$A = 2\pi r_o L$$

$$= 2\pi\left(\frac{3.25}{12}\right)(1.0)$$

$$= 1.70 \text{ ft}^2/\text{ft}$$

$$Re = \frac{D_o \dot{m}_o}{\mu_f} = \frac{\rho_f D_o \dot{m}_o}{\mu_f}$$

$$10 \frac{\text{mile}}{\text{hr}} \left(\frac{5280 \text{ ft}}{\text{mile}} \right) = 52800 \frac{\text{ft}}{\text{hr}}$$

$$Re = \frac{\left(\frac{6.5}{12} \right) (52800) (.084)}{.04}$$

$$M_f = .04 \frac{\text{lb}_m}{\text{hr-ft}}$$

$$= 60000$$

$$\frac{hD_o}{k_f} = 170 \text{ (see pg 7)}$$

$$h = \frac{170 (.0135)}{(6.5/12)}$$

$$= 4.24 \text{ Btu/hr-ft}^2\text{-}^\circ\text{F}$$

To account for radiation, say $h = 4.5 \frac{\text{Btu}}{\text{hr-ft}^2\text{-}^\circ\text{F}}$

$$\therefore .04(10.15)(325 - T_o) = 4.5(1.70)(T_o - 15)$$

$$131.95 - .406T_o = 7.65T_o - 114.75$$

$$8.06T_o = 246.7$$

$$T_o = 30.6^\circ\text{F}$$

$$\therefore q = hS(T_i - T_o)$$

$$= .04(10.15)(325 - 30.6)$$

$$= 119.5 \frac{\text{Btu}}{\text{hr-ft}}$$

for 60 ft of pipe

$$q = 119.5(60) = 7172 \text{ Btu/hr}$$



∴ Calculate the temp drop of the N₂ inside the pipe

$$q = \dot{m} c_p \Delta T$$

$$7172 = .22(3600)(.25) \Delta T$$

$$\Delta T = 36^\circ \text{F}$$

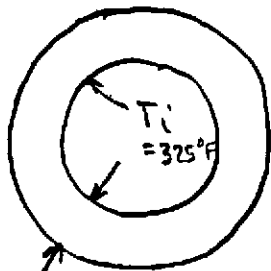
N₂ temp in needs to be

$$\begin{array}{r} 325 \\ + 36 \\ \hline 361^\circ \text{F} \end{array} \quad \text{say } 360^\circ \text{F}$$

//

Short pump

1/2" ϕ pipe
(1.9" o.d.)



1/2" insul

50 gm/sec
(.11 lbm/sec)

$$S = \frac{2\pi(1.0)}{\ln(4.9/1.9)} = 6.63 \text{ ft}$$

$$A = 2\pi \left(\frac{4.9}{2(12)} \right) (1.0) = 1.28 \text{ ft}^2/\text{ft}$$

10 m.p.h. wind

$$Re = \frac{\left(\frac{4.9}{12} \right) (52800) (.084)}{.04} = 45300$$

$$\frac{hD_o}{k_f} = 150 \quad (\text{see pg 7})$$



$$h = \frac{150 (.0135)}{(4.9/12)}$$

$$= 4.96 \text{ Btu/hr-ft}^2\text{-}^\circ\text{F}$$

say 5.5 Btu/hr-ft²-°F

$$kS(T_i - T_o) = hA(T_o - T_{amb})$$

$$.04(6.63)(325 - T_o)$$

$$= 5.5(1.28)(T_o - 15)$$

$$86.19 - .265T_o = 7.04T_o - 105.6$$

$$191.8 = 7.305T_o$$

$$T_o = 26.3^\circ\text{F}$$

$$q = kS(T_i - T_o)$$

$$= .04(6.63)(325 - 26.3)$$

$$= 79.21 \text{ Btu/hr-ft}$$

for 60 ft of pipe

$$q = 60(79.21) = 4753 \text{ Btu/hr}$$

∴ Temp drop of N₂:

$$q = \dot{m}c_p\Delta T$$

$$4753 = .11(3600)(.25)\Delta T$$

$$\Delta T = 48^\circ\text{F}$$

∴ T_{in} must be

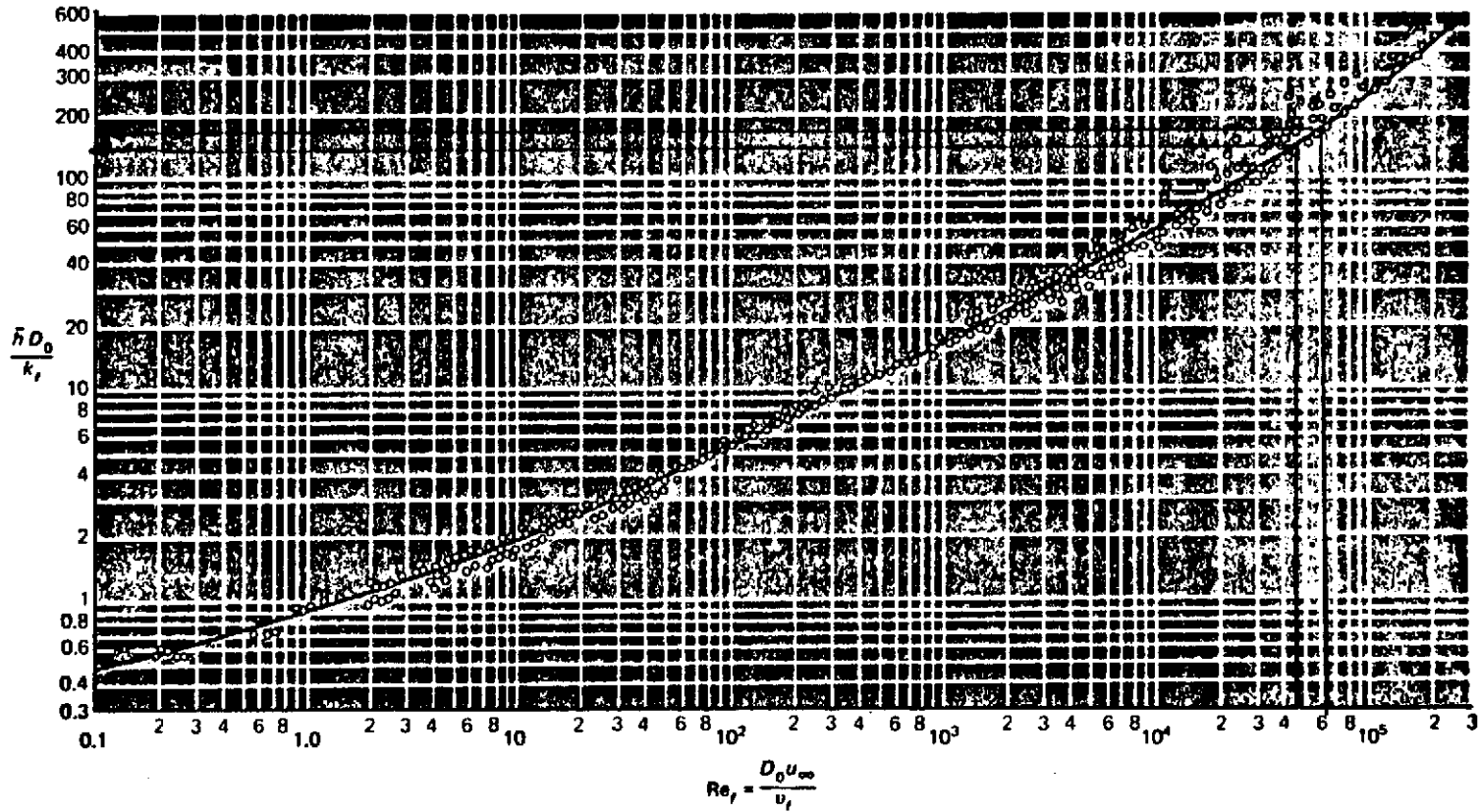
$$\begin{array}{r} 325 \\ + 48 \\ \hline 373 \text{ (say } 375^\circ\text{F)} \end{array}$$





22-141 50 SHEETS
22-142 100 SHEETS
22-144 200 SHEETS

Fig. 6-9 Data for heating and cooling of air flowing normal to single cylinders, from McAdams [10].



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Regen Heater Sizes:

Vaporizer design is based on 20°F approach temp. ∴ the N₂ gas out of the vaporizer will be 15°F - 20°F = -5°F (253 K)

Long pump:

100 gm/sec. flowrate at 253K
raised to 455K (360°F)

$$Q = \left(100 \frac{\text{gm}}{\text{sec}}\right) (472.8 - 262) \frac{\text{j}}{\text{gm}}$$
$$= 21080 \text{ watts}$$

(Heater size approx 25 kW)

100 gm/sec → 10572 SCFH (say 10600 SCFH)

Short pump:

50 gm/sec. flowrate at 253K raised to
464K (375°F)

$$Q = 50 \frac{\text{gm}}{\text{sec}} (482.3 - 262) \frac{\text{j}}{\text{gm}}$$
$$= 11015 \text{ watts (Heater size approx 12 kW)}$$

50 gm/sec → say 5300 SCFH



Time to vaporize LN₂:

Long pump: ~ 1700 lbm of LN₂ (772,700 gm)
Purge gas flow = 100 gm/sec.
@ 253K

$$(\dot{m} \Delta h)_{N_2 \text{ gas}} = \dot{m} h_{fg}$$

$$\dot{m}_{\text{vaporized}} = \frac{(\dot{m} \Delta h)_{N_2 \text{ gas}}}{h_{fg}}$$

$$= \frac{(100 \text{ gm/sec})(262 - 79.6) \text{ J/gm}}{(78.4 + 118.1) \text{ J/gm}}$$

$$= 92.8 \text{ gm/sec. (.204 lbm/sec)}$$

∴ Time to vaporize is:

$$t = \frac{1702 \text{ lbm}}{.204 \text{ lbm/sec}}$$

$$= 8324 \text{ sec (2.3 hr.)}$$

Short pump: ~ 550 lbm of N₂

Purge gas flow = 50 gm/sec.

$$\dot{m}_{\text{vaporized}} = \frac{(50)(262 - 79.6)}{(78.4 + 118.1)}$$

$$= 46.4 \text{ gm/sec (.102 lbm/sec)}$$

∴ Time to vaporize is:

$$t = \frac{550}{.102} = 5392 \text{ sec (1.5 hr.)}$$



Long Pump Regen.
Warmup Time
Winter Conditions

N2 flow (gm/sec)	Cp of N2 (j/gm-K)	N2 in (K)	N2 out (K)	Cp alum. (j/gm-K)	Initial alum. temp (K)	Final alum. temp. (K)	Alum. mass (gm.)	Elapsed time (sec)
50	1.05	253	80	0.357	80	100	1341000	1054.2
50	1.05	253	100	0.481	100	120	1341000	2660.22
50	1.05	253	120	0.58	120	140	1341000	4888.02
50	1.05	253	140	0.654	140	160	1341000	7844.66
50	1.05	253	160	0.713	160	180	1341000	11761.2
50	1.05	253	180	0.76	180	200	1341000	17079.7
50	1.05	253	200	0.797	200	220	1341000	24761.9
100	1.05	436	220	0.826	220	240	1341000	25738.7
100	1.05	436	240	0.849	240	260	1341000	26845.1
100	1.05	436	260	0.869	260	280	1341000	28106.3
100	1.05	436	280	0.886	280	300	1341000	29557
100	1.05	436	300	0.902	300	320	1341000	31251.1
100	1.05	436	320	0.918	320	340	1341000	33272.5
100	1.05	436	340	0.934	340	360	1341000	35757.6
100	1.05	436	360	0.934	360	380	1341000	38896.7
100	1.05	436	380	0.934	380	400	1341000	43156.8
100	1.05	436	400	0.934	400	420	1341000	49783.8
100	1.05	436	420	0.934	420	423	1341000	52020.4

Time to vaporize LN2 = 2.3 hours
Total warmup time = 16.75 hours

Short Pump Regen.
Warmup Time
Winter Conditions

N2 flow (gm/sec)	Cp of N2 (j/gm-K)	N2 in (K)	N2 out (K)	Cp alum. (j/gm-K)	Initial alum. temp (K)	Final alum. temp. (K)	Alum. mass (gm.)	Elapsed time (sec)
50	1.05	253	80	0.357	80	100	398000	312.879
50	1.05	253	100	0.481	100	120	398000	789.537
50	1.05	253	120	0.58	120	140	398000	1450.73
50	1.05	253	140	0.654	140	160	398000	2328.25
50	1.05	253	160	0.713	160	180	398000	3490.66
50	1.05	253	180	0.76	180	200	398000	5069.16
50	1.05	253	200	0.797	200	220	398000	7349.16
50	1.05	436	220	0.826	220	240	398000	7928.97
50	1.05	436	240	0.849	240	260	398000	8585.73
50	1.05	436	260	0.869	260	280	398000	9334.34
50	1.05	436	280	0.886	280	300	398000	10195.5
50	1.05	436	300	0.902	300	320	398000	11201.1
50	1.05	436	320	0.918	320	340	398000	12400.9
50	1.05	436	340	0.934	340	360	398000	13876.1
50	1.05	436	360	0.934	360	380	398000	15739.4
50	1.05	436	380	0.934	380	400	398000	18268.2
50	1.05	436	400	0.934	400	420	398000	22201.8
50	1.05	436	420	0.934	420	423	398000	23529.5

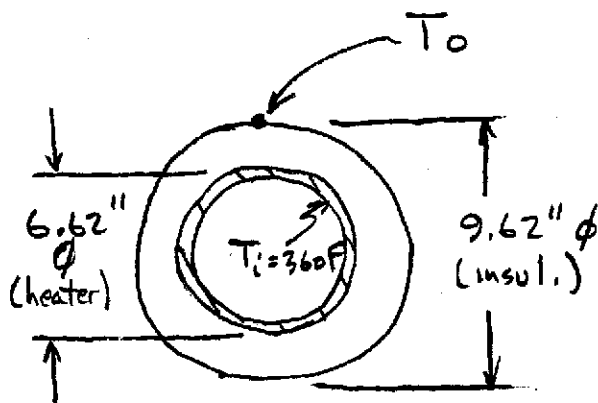
Time to vaporize LN2 = 1.5 hours
Total warmup time = 8.036 hours

Personnel Protection:

Calculate heater insulation outside surface temperature under extreme conditions.

Outside ambient = 96°F dry bulb

Assume light breeze (5 m.p.h.) and heater has been powered up beyond normal requirements. (Heater will need to operate slightly above 150 C (302 F) for pump regeneration.) Assume 360 F heater temp.



$T_{amb} = 96^{\circ}F$
Heater Cross-section

$$k_{insul} = .04 \frac{BTU}{hr \cdot ft \cdot F}$$

(fiberglass)

$$\epsilon \approx 0.8$$

Energy in = energy out

$$kS(T_i - T_o) = hA(T_o - T_a) + \sigma A\epsilon(T_o^4 - T_{amb}^4)$$



$$S = \frac{2\pi L}{\ln(d_o/d_i)}$$

$$= \frac{2\pi(11.0)}{\ln(9.62/6.62)} = 16.81 \text{ ft. (per unit ft. of length)}$$

$$A = \pi d_o L$$

$$= \pi \left(\frac{9.62}{12}\right) (11.0) = 2.52 \text{ ft}^2/\text{ft.}$$

For 5 mph wind

$$5 \text{ mph (5280)} = 26400 \text{ ft/hr.}$$

$$Re = \frac{\rho_f D u_\infty}{\mu_f}$$

$$= \frac{.07 (9.62/12) (26400)}{.046}$$

$$= 32000$$

From pg 7, $\frac{h D_o}{k_f} = 125$

$$h = \frac{125 (.0154)}{(9.62/12)}$$

$$h = 2.4 \text{ Btu/hr-ft}^2\text{-}^\circ\text{F}$$



$$\begin{aligned} \therefore .04 (16.81) (360 - T_0) \\ = 2.4 (2.52) (T_0 - T_{amb}) + \\ (.1714 \times 10^{-8}) (2.52) (0.8) \left((T_0 + 460)^4 - 554^4 \right) \end{aligned}$$

$$.672 (360 - T_0) = 6.05 (T_0 - 96) + 3.46 \times 10^{-9} \left((T_0 + 460)^4 - 554^4 \right)$$

Solution by trial & error

T_0 (°F)	L.H.S. (Btu/hr)	R.H.S. (Btu/hr)
110	168	124
115	164.6	167.2 ← close

∴ Surface of insulation will be approx 115°F
 & 1 1/2" thick insulation is adequate for
 personnel protection.

Attachment 1.

Table C-1 (Cont.)

STATE AND STATION	WINTER		SUMMER			STATE AND STATION	WINTER		SUMMER		
	Latitude	DB 97%	DB 2%	WB 2%	Outdoor Daily Range		Latitude	DB 97%	DB 2%	WB 2%	Outdoor Daily Range
Lubbock AP	33	15	97	72	26	Everett-Paine AFB	47	24	78	65	20
Lufkin AP	31	28	86	80	20	Kennewick	46	15	86	66	30
McAllen	26	38	100	79	21	Longview	46	24	86	66	30
Midland AP	32	23	98	73	26	Moss Lake, Lamson AFB	47	-1	93	66	32
Mineral Wells AP	32	22	100	77	22	Olympia AP	47	25	83	65	32
Palustrine CO	31	25	97	79	20	Port Angeles	48	28	73	68	18
Pampa	35	11	98	72	26	Seattle-Boeing Fld.	47	27	80	65	24
Pecos	31	19	100	71	27	Seattle CO	47	32	79	65	19
Plainview	34	14	98	72	26	Seattle-Tacoma AP	47	4	81	64	22
Port Arthur AP	30	33	92	80	19	Spokane AP	47	4	90	64	28
San Angelo						Tacoma-McChord AFB	47	24	81	66	22
Goodfellow AFB	31	25	99	75	24	Walla Walla AP	46	16	96	68	27
San Antonio AP	29	30	97	77	19	Wenatchee	47	9	92	66	32
Sherman-Perrin AFB	33	23	99	78	22	Yakima AP	46	10	92	67	36
Snyder	32	19	100	74	26						
Temple	31	27	99	78	22	WEST VIRGINIA					
Tyler AP	32	24	97	79	21	Beckley	37	6	88	73	22
Vernon	34	18	101	76	24	Bluefield AP	37	10	86	73	22
Victoria AP	28	32	96	79	18	Charleston AP	38	14	90	75	20
Waco AP	31	26	99	78	22	Clarksburg	39	7	90	75	21
Wichita Falls AP	34	19	100	76	24	Elkins AP	38	5	84	73	22
						Huntington CO	38	14	93	76	22
UTAH						Martinsburg AP	39	10	94	77	21
Cedar City AP	37	6	91	64	32	Morgantown AP	39	7	88	74	22
Logan	41	7	91	65	33	Parkersburg CO	39	12	91	76	21
Moab	38	16	98	65	30	Wheeling	40	9	89	75	21
Ogden CO	41	11	92	65	33						
Price	39	7	91	64	33	WISCONSIN					
Provo	40	6	93	66	32	Appleton	44	-6	87	74	23
Richfield	38	3	92	65	34	Ashland	46	-17	83	71	23
St. George CO	37	26	102	70	33	Beloit	42	-3	90	76	24
Salt Lake City AP	40	9	94	66	32	Eau Claire AP	44	-11	88	74	23
Vernal AP	40	-6	88	63	32	Fond du Lac	43	-7	87	74	23
						Green Bay AP	44	-7	85	73	23
VERMONT						Le Cross AP	43	-8	88	76	22
Barre	44	-13	84	72	23	Madison AP	43	-5	88	75	22
Burlington AP	44	-7	85	73	23	Maritowoc	44	-1	86	74	21
Rutland	43	-8	85	73	23	Marinette	45	-4	86	72	20
						Milwaukee AP	43	-2	87	75	21
VIRGINIA						Racine	42	0	88	75	21
Charlottesville	38	15	90	77	23	Shelbygan	43	0	87	74	20
Danville AP	36	17	92	77	21	Stevens Point	44	-12	87	73	23
Fredericksburg	38	14	92	78	21	Waukesha	43	-2	88	75	22
Harrisonburg	38	9	90	77	23	Wausau AP	44	-14	86	72	23
Lynchburg AP	37	19	92	76	21						
Norfolk AP	36	23	91	78	18	WYOMING					
Petersburg	37	18	94	79	20	Casper AP	42	-5	90	62	31
Richmond AP	37	18	93	78	21	Cheyenne AP	41	-2	86	62	30
Roanoke AP	37	18	91	75	23	Cody AP	44	-9	87	60	32
Staunton	38	12	90	77	23	Evanson	41	-8	82	57	32
Winchester	39	10	92	76	21	Lander AP	42	-12	90	62	32
						Laramie AP	41	-2	80	59	28
WASHINGTON						Newcastle	43	-5	89	67	30
Aberdeen	47	27	80	61	16	Ramvins	41	-11	84	61	40
Bellingham AP	48	18	74	65	19	Rock Springs AP	41	-1	84	57	32
Bremerton	47	29	81	66	20	Sheridan AP	44	-7	92	65	32
Ellensburg AP	47	6	89	65	34	Torrington	42	-7	92	67	30

EXPLANATION OF DESIGN CONDITIONS:

WINTER - 97% indicates that the temperature will be at or above the design temperature shown 97% of the time.

SUMMER - 2% indicates that the temperature will exceed the design temperature shown only 2% of the time.

OUTDOOR DAILY RANGE - The outdoor daily range of DB temperatures is the difference between the average maximum and average minimum temperatures during the warmest month at each location. Refer to page 39 when outdoor daily range is other than 20°.

22-141 50 SHEETS
 22-142 100 SHEETS
 22-144 200 SHEETS

